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Joint Research Centre

## Migration modelling

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# Practical guidelines migration modelling

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## JRC TECHNICAL REPORTS

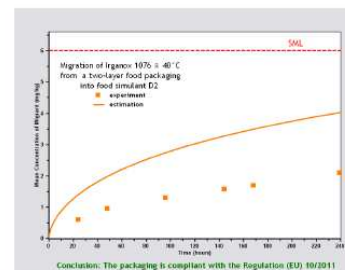
Practical guidelines on the application of migration modelling for the estimation of specific migration

*In support of Regulation (EU)  
No 10/2011 on plastic food  
contact materials*

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2015

$$\frac{C_i^{n+1} - C_i^n}{\Delta t} = D \frac{C_{i+1}^n - 2C_i^n + C_{i-1}^n}{h^2}$$



EUR 27529 EN

# Regulation (EC) No 10/2012

## Compliance test

- Verification method
- Screening method

- Overall migration
- Residual content
- Migration modelling
- Food simulant substitutes

No underestimation of modelled specific migration (section 2.2.3 of Annex V)

FCM not yet in contact

Art. 18.3

Compliant?

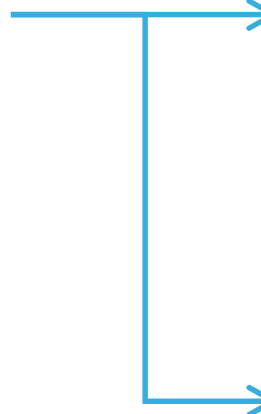
yes

OK

no

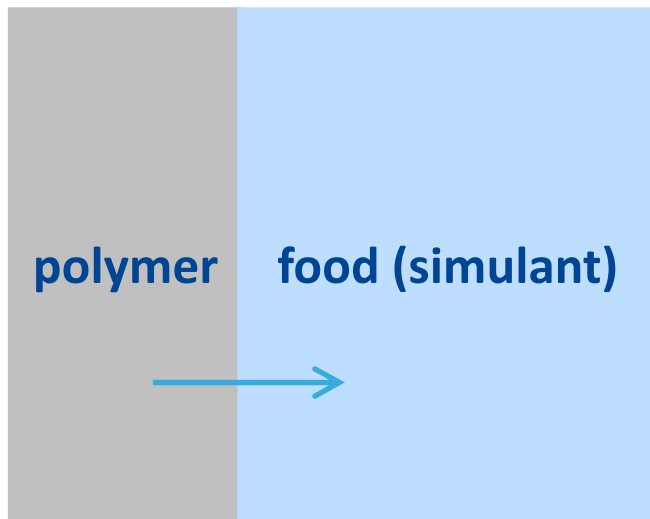
# Migration

- Diffusion
- Convection
- Evaporation
- Reaction
- Partitioning


$$\frac{\partial c}{\partial t}$$

**Diffusion is a good simplification for most food contact materials**

## Monolayer – one dimensional



### Fick's second law of diffusion

$$\frac{\partial c_P}{\partial t} = D_P \frac{\partial^2 c_P}{\partial x^2}$$

### At equilibrium ( $t=\infty$ )

$$K_{P,F} = \frac{c_{P,\infty} \rho_P}{c_{F,\infty} \rho_F}$$

## Boundary conditions

- Constant thickness of polymer film
- Polymer film in contact with finite volume of food (simulant) and contact area
- Migrant homogeneously distributed in polymer at  $t=0$
- Neglecting mass transfer resistance at food (simulant) side
- Migrant homogeneously distributed in food (simulant) at  $t>0$
- No interaction between polymer and food (simulant)
  - ✓ no swelling of polymer
- Diffusion coefficient of migrant in polymer is constant
  - ✓ in place and time
- No migrant in food (simulant) at  $t=0$
- The amount of migrant in polymer + food (simulant) is constant

$$m_{F,\infty} + m_{P,\infty} = m_{P,0}$$

## Mass transfer equation

- Analytical solution

$$\frac{m_{F,t}}{A} = c_{P,0} \rho_P d_P \left( \frac{\alpha}{1+\alpha} \right) \left[ 1 - \sum_{n=1}^{\infty} \frac{2\alpha(1+\alpha)}{1+\alpha+\alpha^2 q_n^2} \exp\left( -q_n^2 \frac{D_P}{d_P^2} t \right) \right]$$

$$\alpha = \frac{1}{K_{P,F}} \frac{V_F}{V_P} = \frac{c_{F,\infty}}{c_{P,\infty}} \frac{\rho_F}{\rho_P} \frac{V_F}{V_P} = \frac{m_{F,\infty}}{m_{P,\infty}}$$

$$\tan q_n = -\alpha q_n$$

- Maximum concentration in polymer

$$MIC = SML \frac{V_F \rho_F}{A} \left\{ \rho_P d_P \left( \frac{\alpha}{1+\alpha} \right) \left[ 1 - \sum_{n=1}^{\infty} \frac{2\alpha(1+\alpha)}{1+\alpha+\alpha^2 q_n^2} \exp\left( -q_n^2 \frac{D_P}{d_P^2} t \right) \right] \right\}^{-1}$$

## Disadvantages of analytical solution

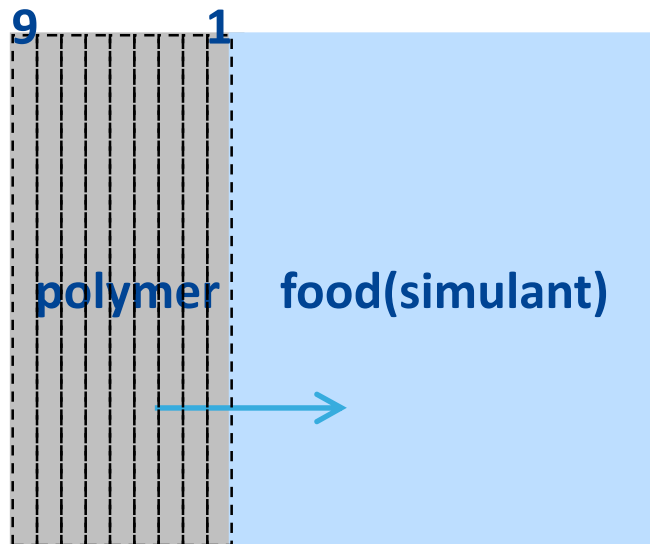
- Only monolayer
- Only mean concentrations in polymer and food (simulant)
- No successive contact cycles possible
  - ✓ Repeated use articles

### *Alternative*

- Numerical solutions
  - ✓ e.g. finite element or finite differences algorithms
  - ✓ Analytical solution serves as reference for validation



## Multi-layer – one dimensional



### Fick's second law of diffusion

$$\frac{\partial c_P}{\partial t} = D_P \frac{\partial^2 c_P}{\partial x^2} \quad \text{For each layer}$$

### At equilibrium ( $t=\infty$ )

$$K_{P_n, F} = \frac{c_{P_n, \infty} \rho_{P_n}}{C_{F, \infty} \rho_F}$$

$$K_{P_{n+1}, P_n} = \frac{c_{P_{n+1}, \infty} \rho_{P_{n+1}}}{c_{P_n, \infty} \rho_{P_n}}$$

# Estimation of diffusion coefficient

## Different approaches

- Arrhenius

$$D_p = D_0 \exp\left(\frac{-E_A}{RT}\right)$$

- Estimation (Piringer)

$$D_p^* = \exp\left( A_p^* - 0.1351M_r^{2/3} + 0.003M_r - \frac{10454R}{RT} \right) \quad (\text{m s}^{-2})$$

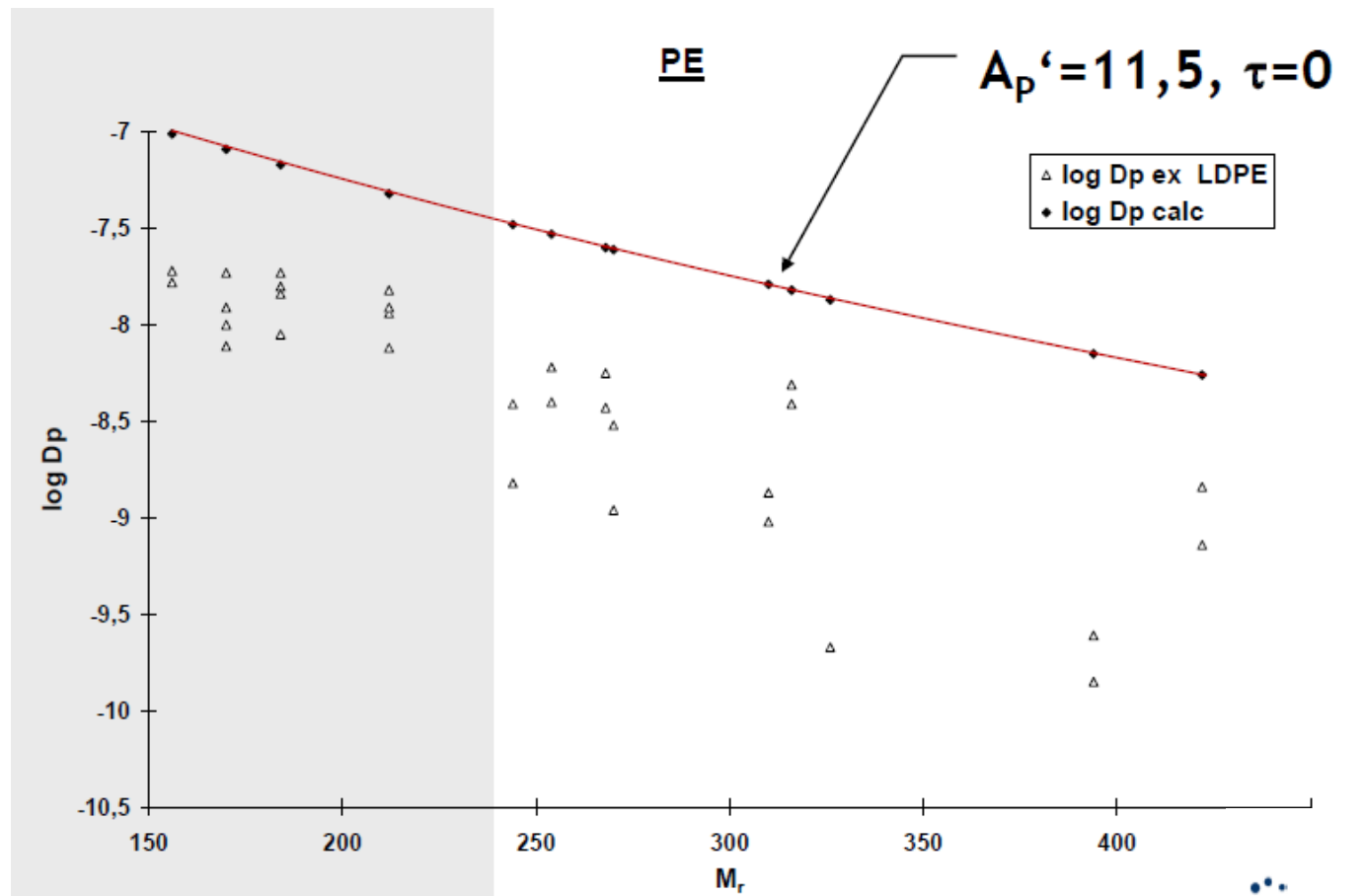
Reference activation energy

$$A_p^* = A_p^* - \frac{\tau}{T}$$

Polymer specific temperature constant

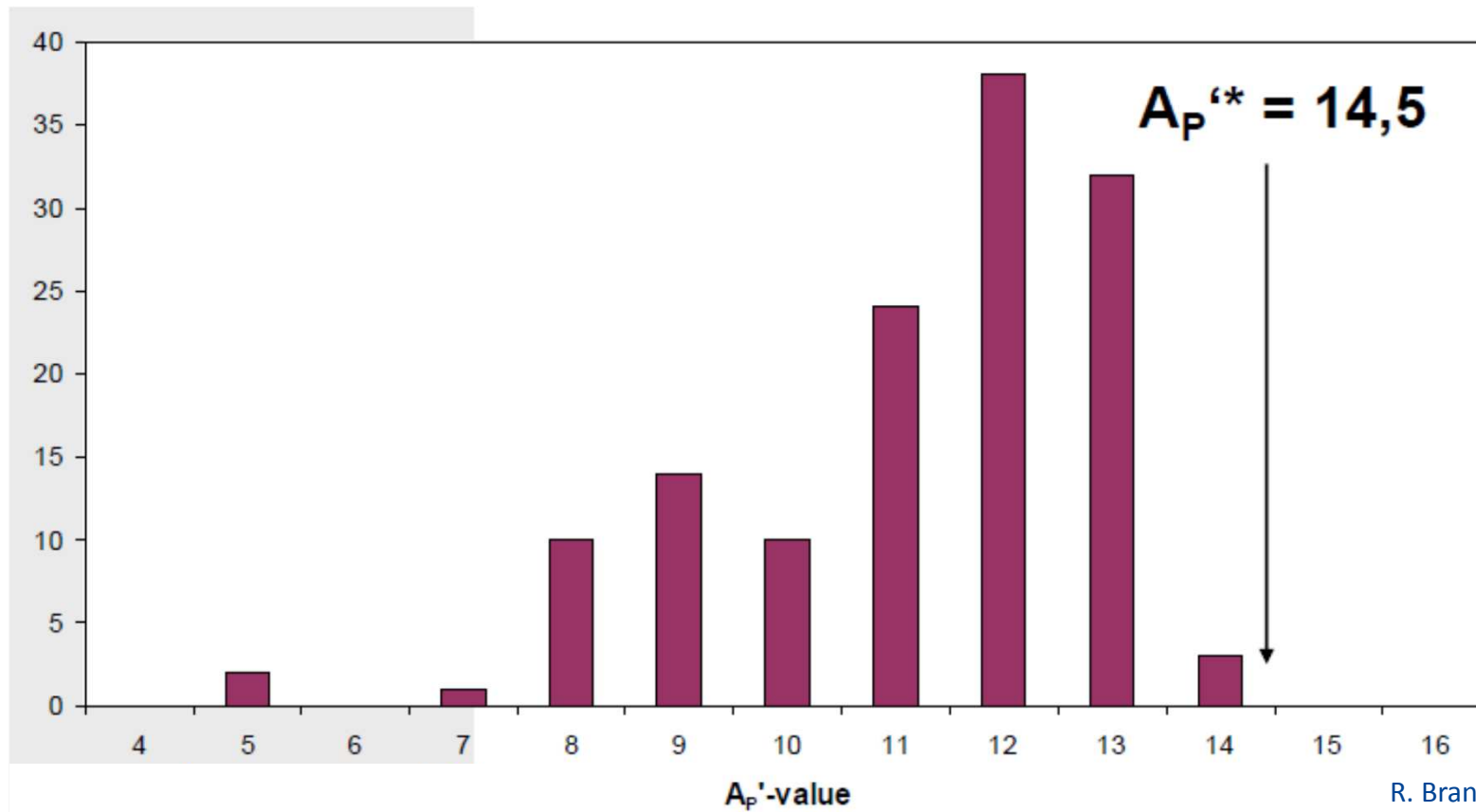
Polymer specific constant

## Estimation of $A_p'$ for each T



R. Brandsch, 2010

## Estimation of $A_p'^*$



R. Brandsch, 2010

## Applicability for polyolefins

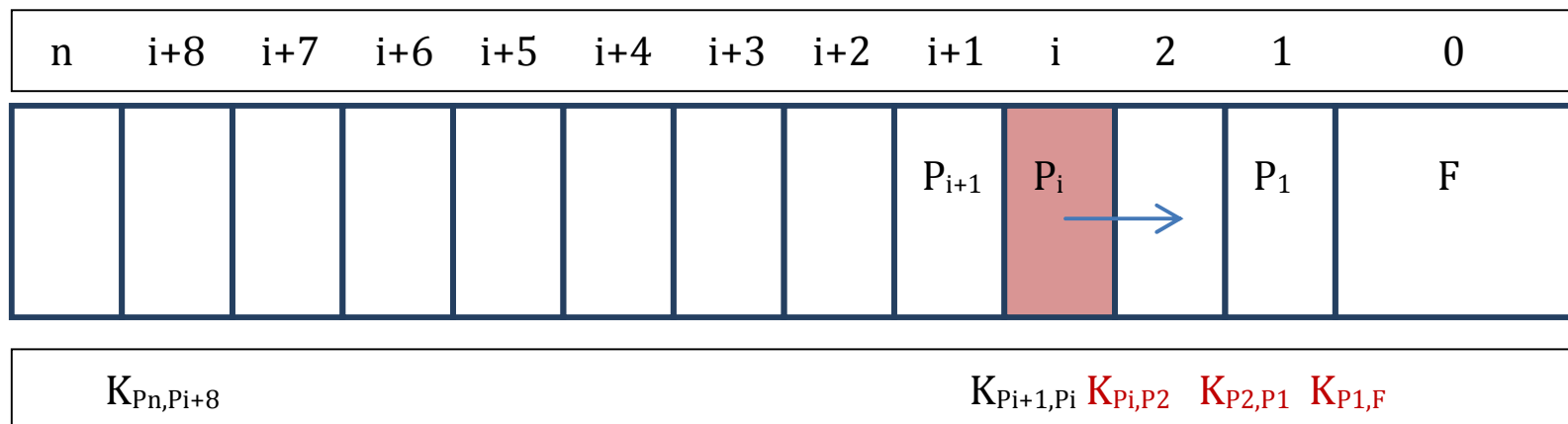
$$c_{P,0} < 1\%$$

$K_{P,F} = 1$  for high solubility of migrant in food.

$K_{P,F} = 1000$  for low solubility of migrant in food.

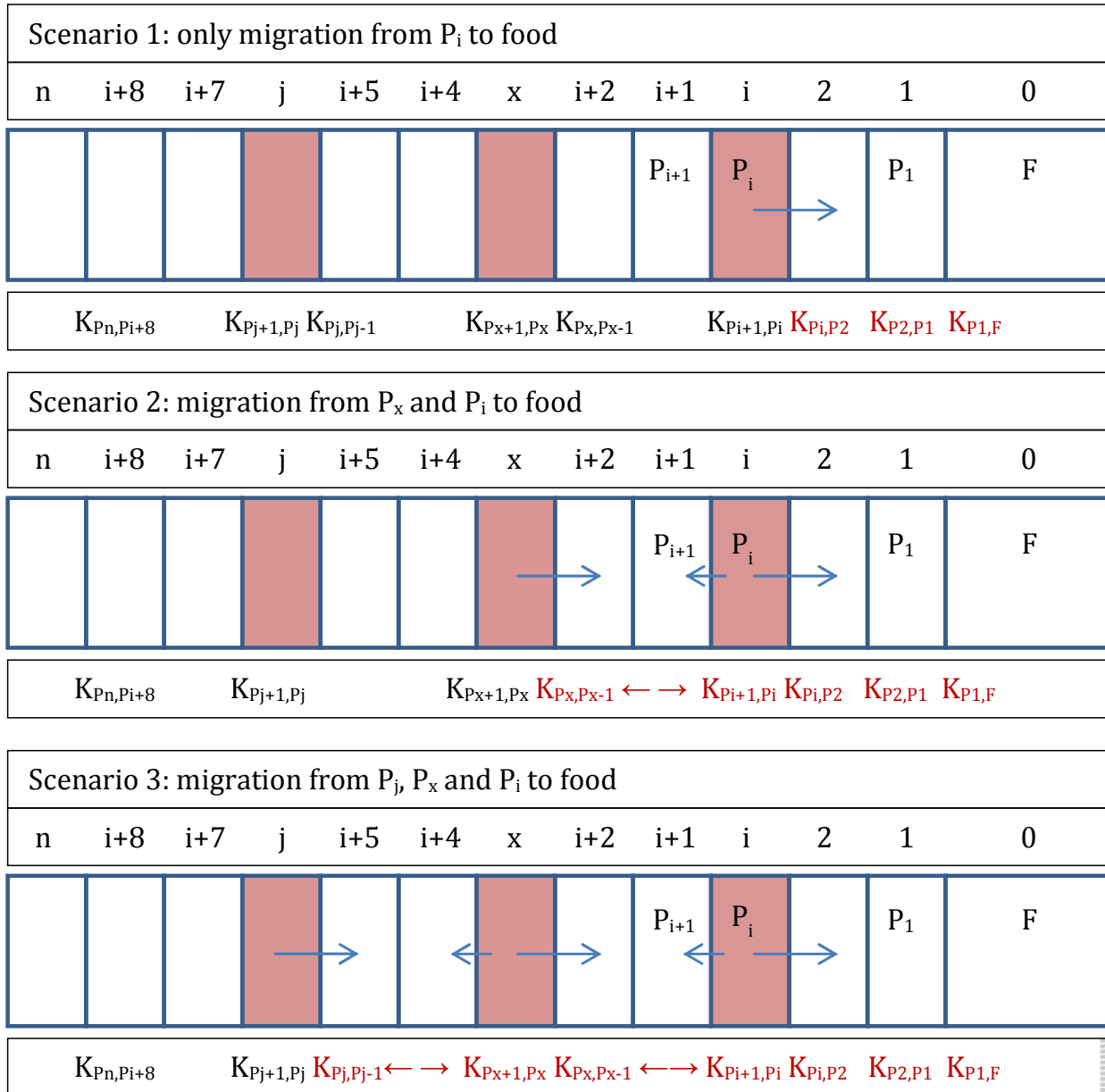
Polymer	T (° C)	M <sub>r</sub> (g/mol)	A <sub>p</sub> '*	τ (K)
LDPE	≤80	30 - 2000	11.5	0
LLDPE	≤100	30 - 2000		
HDPE	≤90	30 - 2000	14.5	1577
PP (homo)	≤120	30 - 2000	13.1	1577
PP (random)	≤120	30 - 2000		
PP (rubber)	≤100	30 - 2000	11.5	0

## Multi-layer: worst case scenario



- Forced specific migration of migrant in one layer (i) to food.
- K in black is **0.001**
- K in red is **1**

# Multi-layer: worst case scenario's



## Substances eligible for migration modelling

- All organic, non-gaseous substances with a well-defined molecular mass, soluble in the polymeric matrix
- All organic substances known to deliberately bloom out from some polymeric materials, e.g. antistatic or antifogging agents incorporated in polyolefines, at levels where blooming does not occur
- All specific substances in a mixture, typically derived from natural sources like fats and oils, rosins, waxes, starch, proteins, cellulose, cotton, with a well defined molecular mass below 2000 g/mol



## Substances not eligible for migration modelling

- **All organic substances known to deliberately bloom out from some polymeric materials, e.g. antistatic or antifogging agents incorporated in polyolefines, at levels where blooming occurs**
- **All organic mixtures with undefined molecular mass, typically derived from natural sources like fats and oils, rosins, waxes, starch, proteins, cellulose, cotton**
- **All inorganic substances, metals, metal oxides, metal salts, etc.**

## Crucial information needed for migration modelling

- **Polymer identity**
- **Potential substances that can migrate**
  - ✓ e.g. additives, residual amounts of monomers
- **Initial concentrations**
- **“worst-case” intended use**
  - ✓ type of food
  - ✓ maximum temperature
  - ✓ maximum packaging time
  - ✓ Intended highest surface-to-volume ratio

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